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**SAARC  
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**Online Capacity Building of SAARC Professionals on  
Commercial Scale Biogas Plants  
August 23-27, 2021**



# Fundamentals on Biogas Production Process

**Aug. 24, 2021, 2:30 – 3:25 pm**

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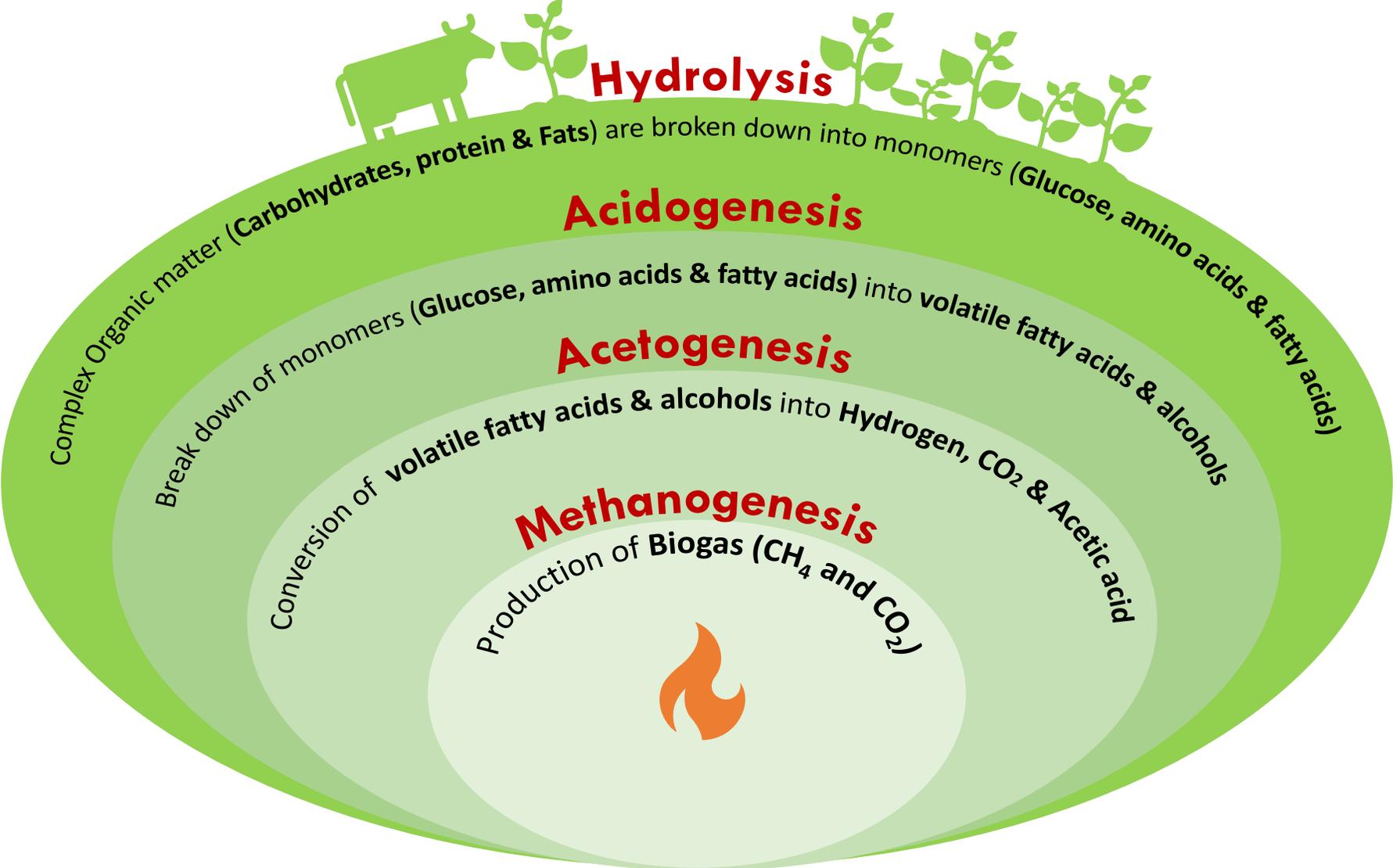
# Contents

- ❑ Biogas production process: four steps involved
- ❑ General biochemical aspects of the biogas production process
- ❑ Process parameters for substantial biogas production
- ❑ Problems associated with biogas production and troubleshooting
- ❑ Recent advances in biogas production technology

## Learning objective

- To learn the fundamentals on biogas production process, problems associated with the biogas process and possible remedial actions.

# Biogas production...



# Biochemical aspect...

## Hydrolysis

*Protein*  
*carbohydrate*  
*fats*

Oxidation

*Fatty acids*  
*alcohols*

Acetogenesis

**CH<sub>3</sub>COOH**

*Acetic acid*

**2CH<sub>3</sub>CH<sub>2</sub>OH + CO<sub>2</sub>**

*Ethanol*

**CO<sub>2</sub> + 4H<sub>2</sub>**

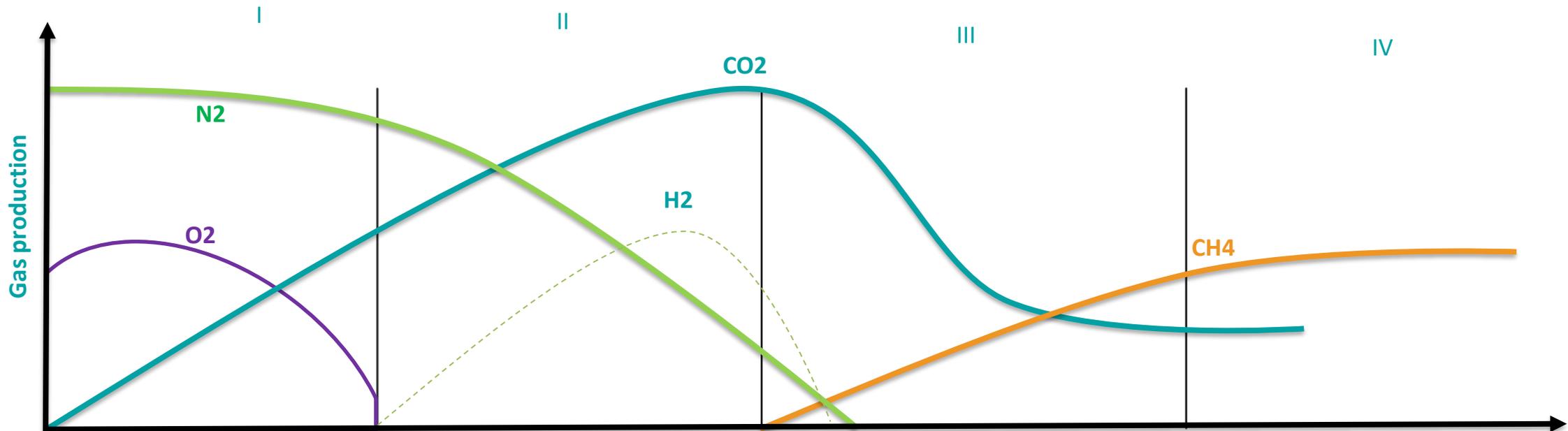
*Carbon dioxide*

Methanogenesis

**CH<sub>4</sub> + CO<sub>2</sub>**

**CH<sub>4</sub> + 2CH<sub>3</sub>COOH**

**CH<sub>4</sub> + 2H<sub>2</sub>O**



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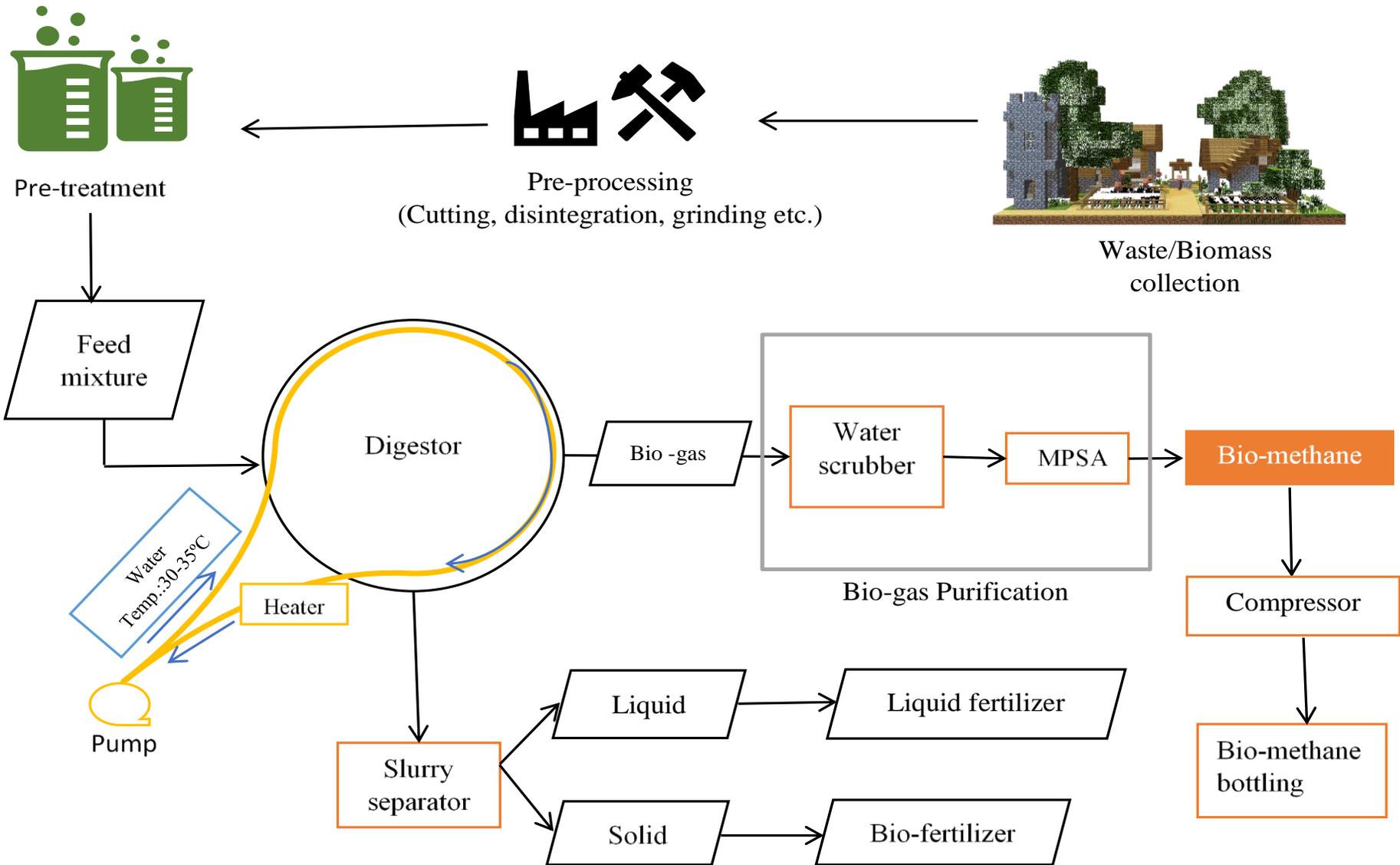
## Composition of Biogas

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Gas	Composition (%)
Methane (CH <sub>4</sub> )	50-75
Carbon dioxide (CO <sub>2</sub> )	25-50
Hydrogen (H <sub>2</sub> )	0-1
Nitrogen (N <sub>2</sub> )	0-10
Hydrogen sulphide (H <sub>2</sub> S)	0-3

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# Biomethane Production Overview



# Waste to Biogas generation potential in Hazaribagh, Bangladesh: A case study

Area of Hazaribagh = 5.65 km<sup>2</sup>

Population density = 32.856/km<sup>2</sup>

## Biomass energy situation in Bangladesh [44].

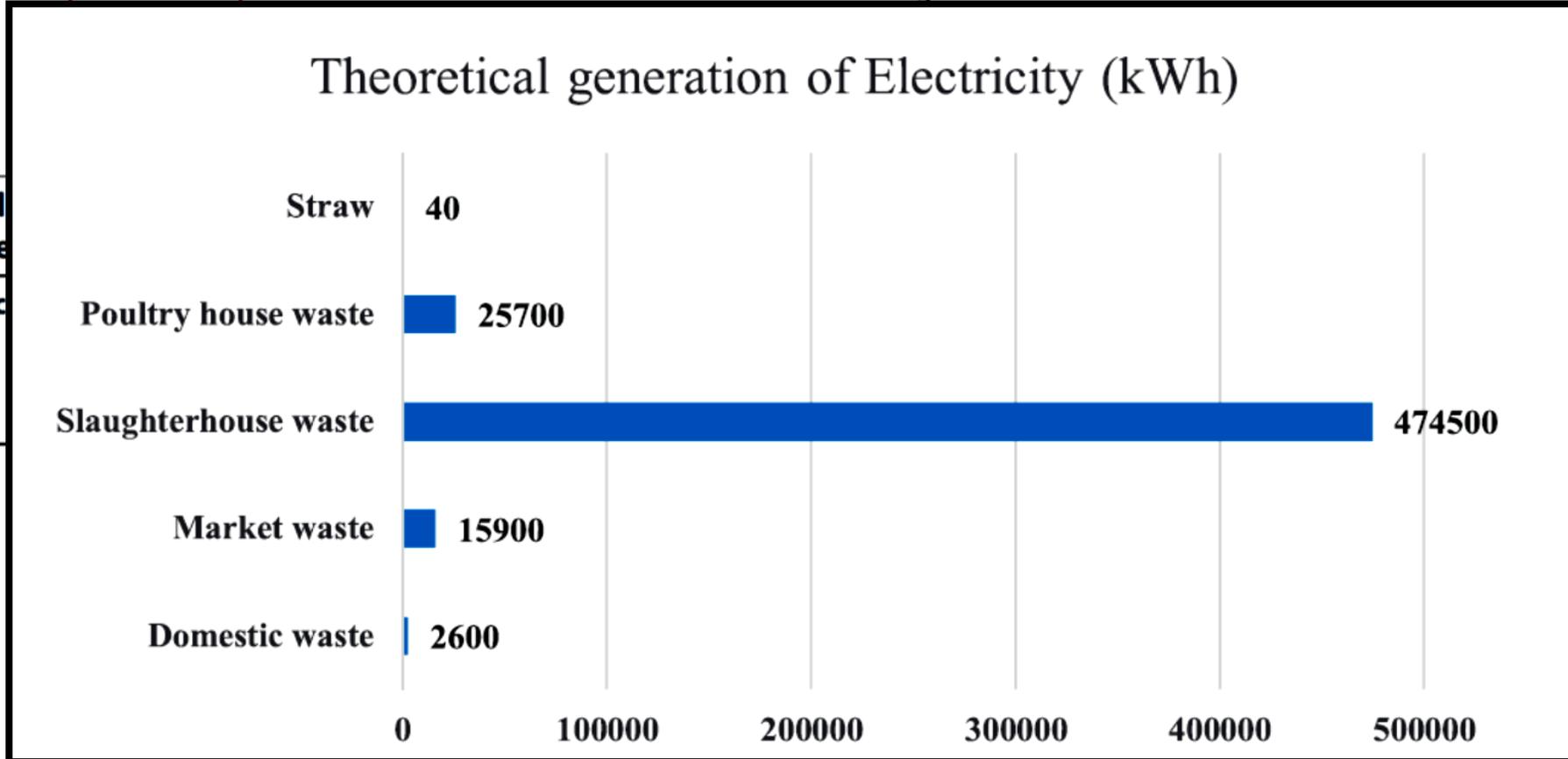
Technology	Potential	Target capacity	Achievement
Domestic biogas system	8.8 million m <sup>3</sup>	1,00,000 biogas plants	Ongoing project
Biomass gasification	300 MW	3 MW	≤1 MW

The estimated  
each substrate

Feedstock source

Domestic waste  
Market waste

Slaughterhouse  
waste  
Poultry house  
waste  
Straw



1 MW

generation from

Theoretical  
generation of  
Electricity (kWh)

2600  
15,900

474,500

25,700

40

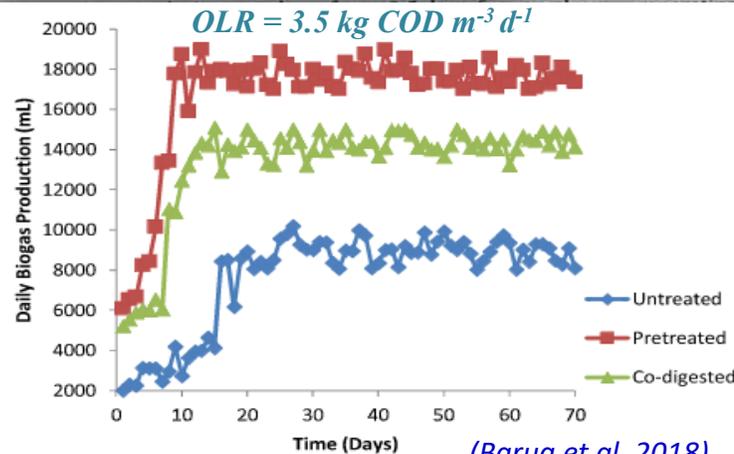
have question marks about the data quality.

(Hasan and Ammenberg 2019)

# From menace to fuel, the turnaround story of water hyacinth



Social entrepreneurs and researchers explain the methods involved in the production of biogas from water hyacinth to Agriculture Minister P. Prasad during a demonstration recently.

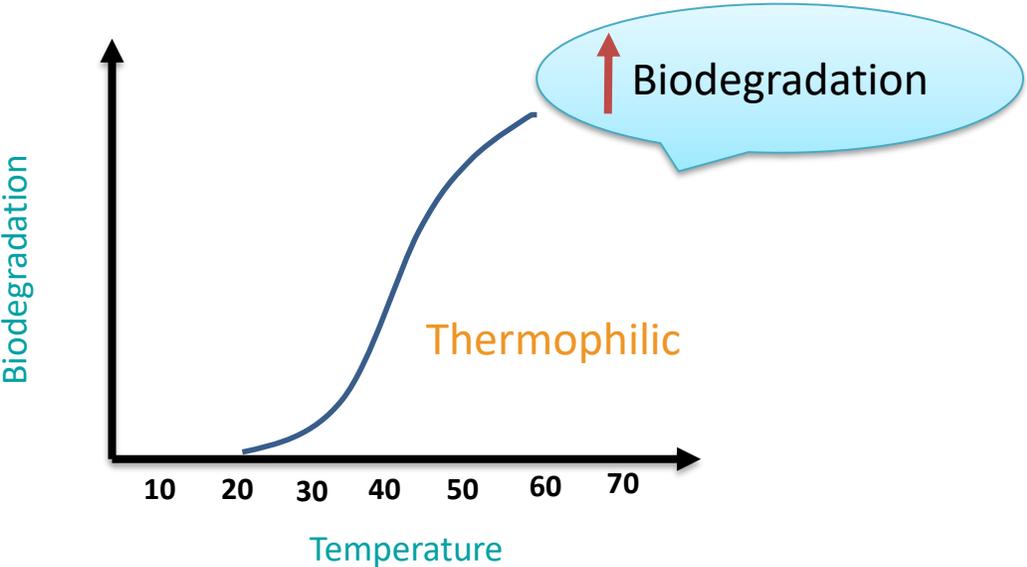
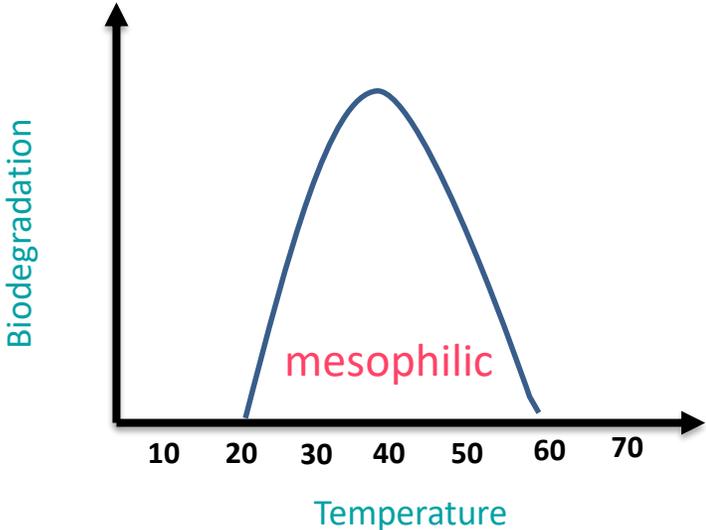


Water content (%)	90
Dry matter (%)	
Cellulose	24
Hemicellulose	30
Lignin	16
Ashes	20
Elemental composition (%)	
C	38.4
H	5.85
O	28.1
N	2.9
S	0.47
P	0.77
K	2.78
Ca	1.32
Na	1.44

(Rathod et al. 2018)

# Process parameters...

## Temperature

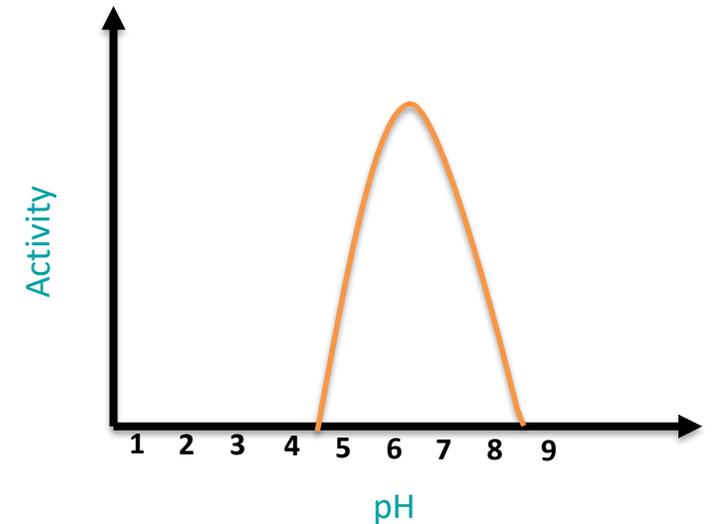


- **Mesophilic range process** - The optimum temperature is 35-37°C
- When the ambient temperature goes down to 10°C, gas production virtually stops.
- Proper insulation of digester helps to increase gas production in the cold season

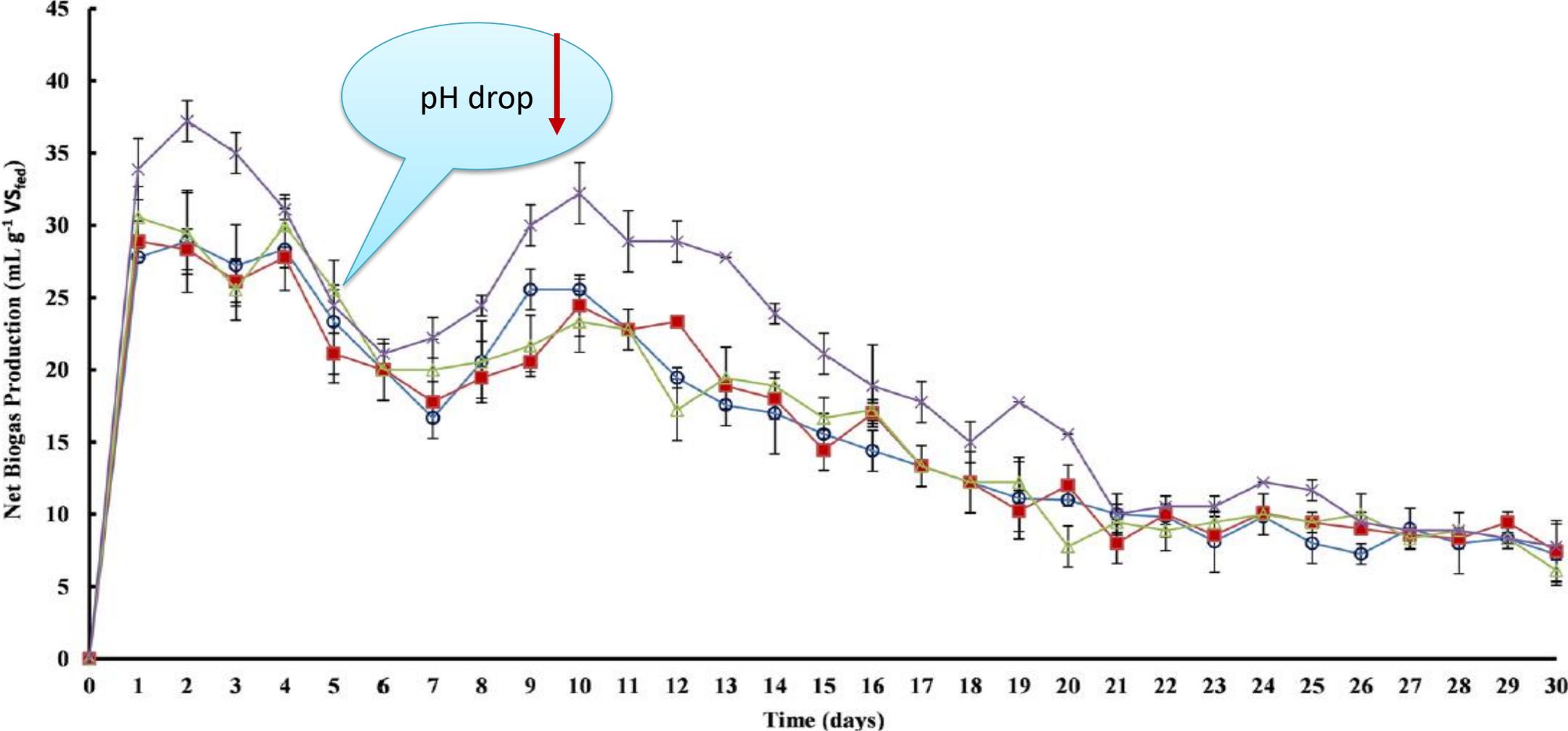
## Cont'd...

# pH

- At early stage of decomposition, organic acid are formed ----- pH drop at about 5.
- The optimum pH of hydrolyzing and acid-forming bacteria is in a range from pH 5.2 to 6.3
- Once microorganism breakdown the organic acids then the pH again rise
- The optimum biogas production is achieved when the pH value of input mixture in the digester is between 6 and 7.
- Methanogenic bacteria are very sensitive to pH and do not thrive below a value of 6.5.



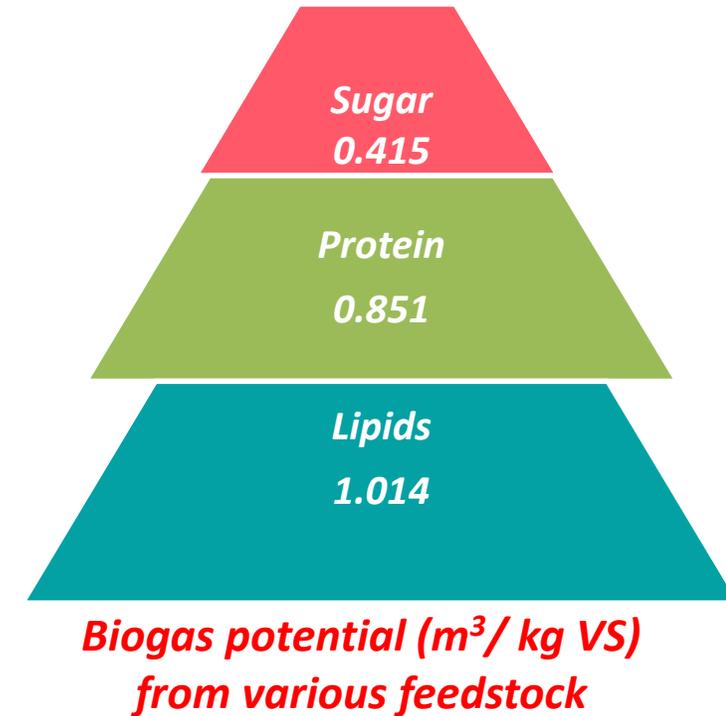
# Cont'd...



## Cont'd...

### Feedstock & Nutrient level

- Carbon--- Energy
- Nitrogen --- Protein synthesis
- Phosphorus and potassium --- cell reproduction and metabolism
- Optimum **C/N ratio = 25:1 – 30:1**
- Macronutrients such as cobalt (Co), nickel (Ni), molybdenum (Mo) and selenium (Se), are vital for the survival of the microorganisms



# Hydraulic Retention Time (HRT)

- HRT is a measure of the average length of time that a soluble compound remains in a constructed bioreactor

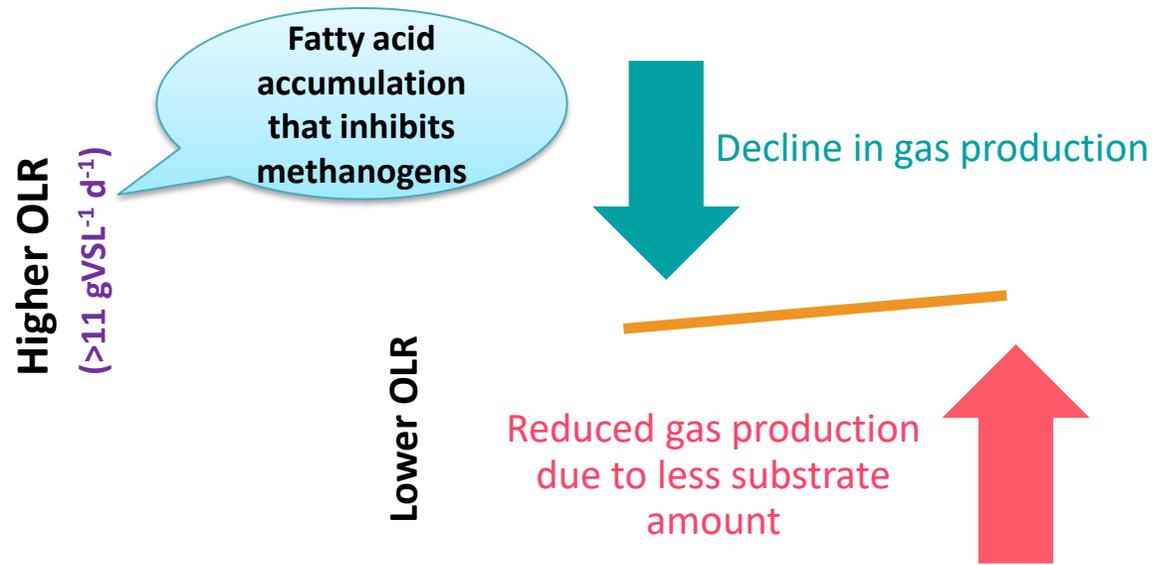
$$HRT(\theta) = \frac{\text{Volume of digester [m}^3\text{]}}{\text{Substrate flow rate [m}^3\text{/d]}} = \frac{V}{Q}$$

- A digester must have a volume of 50 to 60 times the slurry added daily.
- Higher the temperature, the lower the retention time.

# Organic loading rate

- Organic loading rate (OLR) is the amount of raw materials fed per unit volume of digester capacity per day.

$$\text{OLR} = \frac{\text{flowrate} \times \text{Substrate concentration}}{\text{Volume}} = \frac{Q \times S}{V}$$



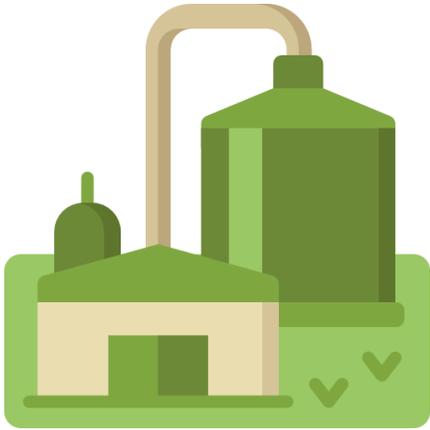
# ● Inhibitors ●

Inhibitor	Inhibitory concentration	Comments
Oxygen	$> 0.1 \text{ mgL}^{-1}$	Inhibition of obligate anaerobic methanogenic archaea
Hydrogen sulphide	$> 50 \text{ mgL}^{-1}$	Inhibitory effect rises with falling pH value
Volatile fatty acids	$> 2,000 \text{ mgL}^{-1}$ HAc (pH = 7.0)	Inhibitory effect rises with falling pH value. High adaptability of bacteria
Ammoniacal nitrogen	$> 2000 \text{ mgL}^{-1}$ $\text{NH}_4^+$ (pH = 7.0)	Inhibitory effect rises with rising pH value and rising temperature. High adaptability of bacteria
Heavy metals	Cu $> 50 \text{ mgL}^{-1}$ Zn $> 150 \text{ mgL}^{-1}$ Cr $> 100 \text{ mgL}^{-1}$	Only dissolved metals have an inhibitory effect. Detoxification by sulphide precipitation
Disinfectants, antibiotics	-	Product-specific inhibitory effect

# Problem associated with biogas production and troubleshooting

## *Causes*

## *Troubleshoot*



Gas yield dropped

- Drop in quality of substrates
- Drop in temperature
- Inhibitory compounds
- Non-homogenous substrates
- Reducing of methanogenic bacteria

- ✓ Assure substrates mixing and quality
- ✓ Check the heating system
- ✓ Check the level of potential inhibitory compounds
- ✓ Add digestate from another digester (if the methanogenic bacteria as drop)

# Cont'd...

Regular measurements of free volatile organic acids (FOS) and total inorganic carbonate (TAC) is the best practice to monitor the stability of the digester

Protocol: <https://mantech-inc.com/blog/automated-fos-tac-ratio-cod-biogas-applications/>

FOS/TAC ratio  
increased

***Causes***

***Troubleshoot***

- A FOS/TAC value of 0.3-0.4 is considered optimal.
- Above this range, there is excessive biomass input
- Below this range, there is too little biomass input

- **VFA rate is too high**
- **Change in feedstock**
- **Lack of buffer**
- **Inhibitory compounds**

- ✓ **Reduce organic loading rate(OLR)**
- ✓ **Use more manure in the mixture**



pH dropped

## *Causes*

- If Feeding rate is too high or variable
- When Operating temperature have changed
- When the agitation is not working

## *Troubleshoot*

- ✓ Reduce the feed substrates until system returns to normal
- ✓ Use only manure until system returns to normal

# Cont'd...

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## *Causes*

- Due to high protein content
- Air is introduced in the digestion
- Variable Temperature

## *Troubleshoot*

- ✓ Reduce or stop feeding
- ✓ Analyze substrates
- ✓ Reduce air introduction



Foaming

# Cont'd...

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Methane  
concentration dropped

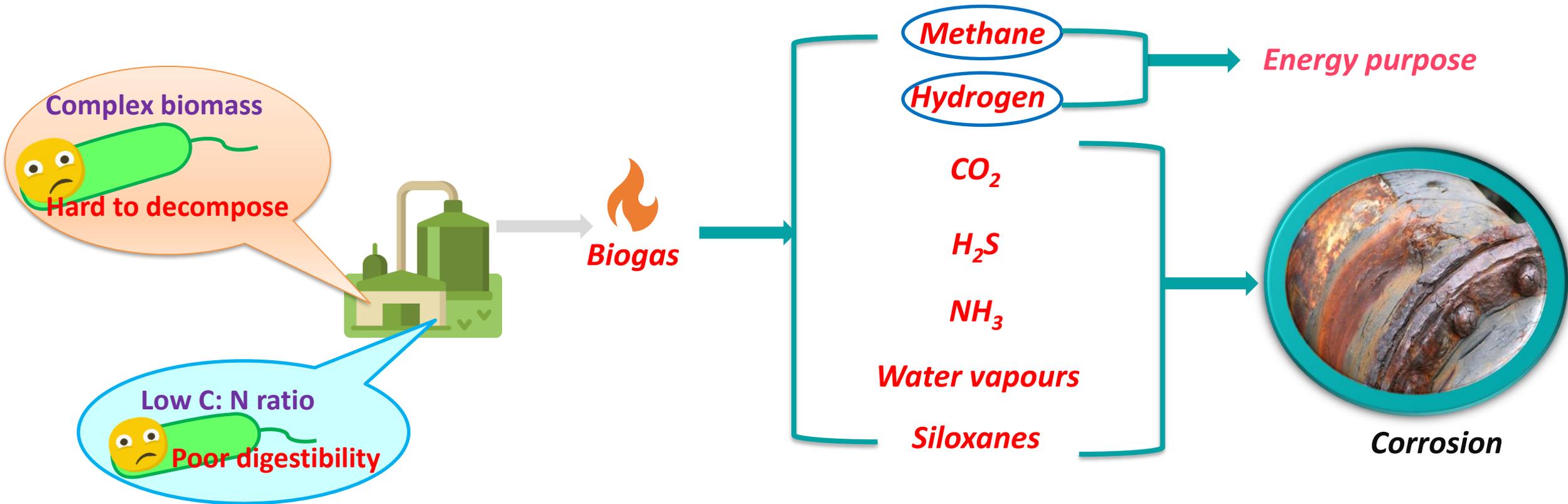
## *Causes*

- Drop in the quality of substrates
- Drop of temperature
- Compounds inhibition

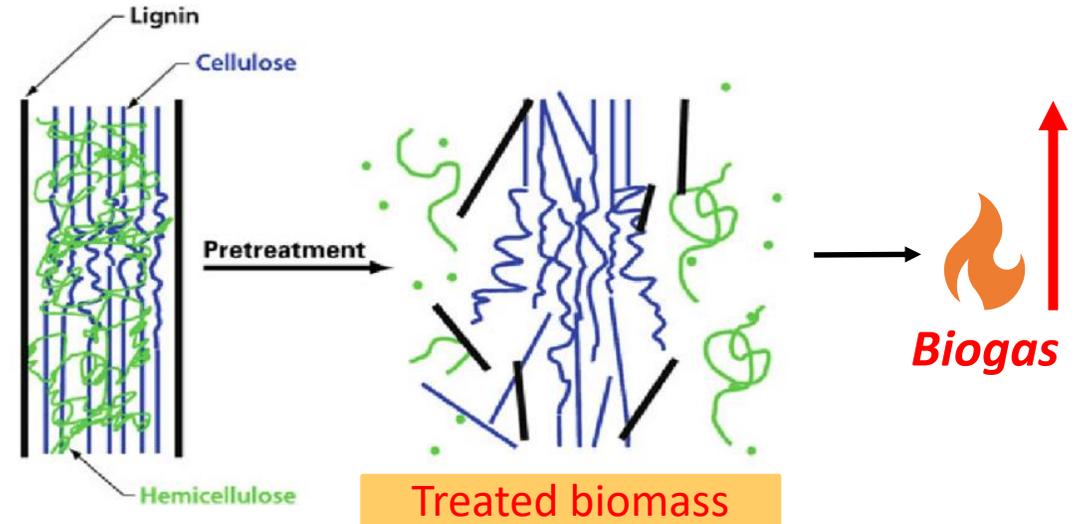
## *Troubleshoot*

- ✓ Assure substrates mixing and quality
- ✓ Check heating system
- ✓ Check level of potential inhibitor compounds

# Recent advances in biogas production



# Biomass pretreatment



Lignocellulosic Biomass = Cellulose (30-65%) + Hemicellulose (10-35%) + Lignin (1-30%)

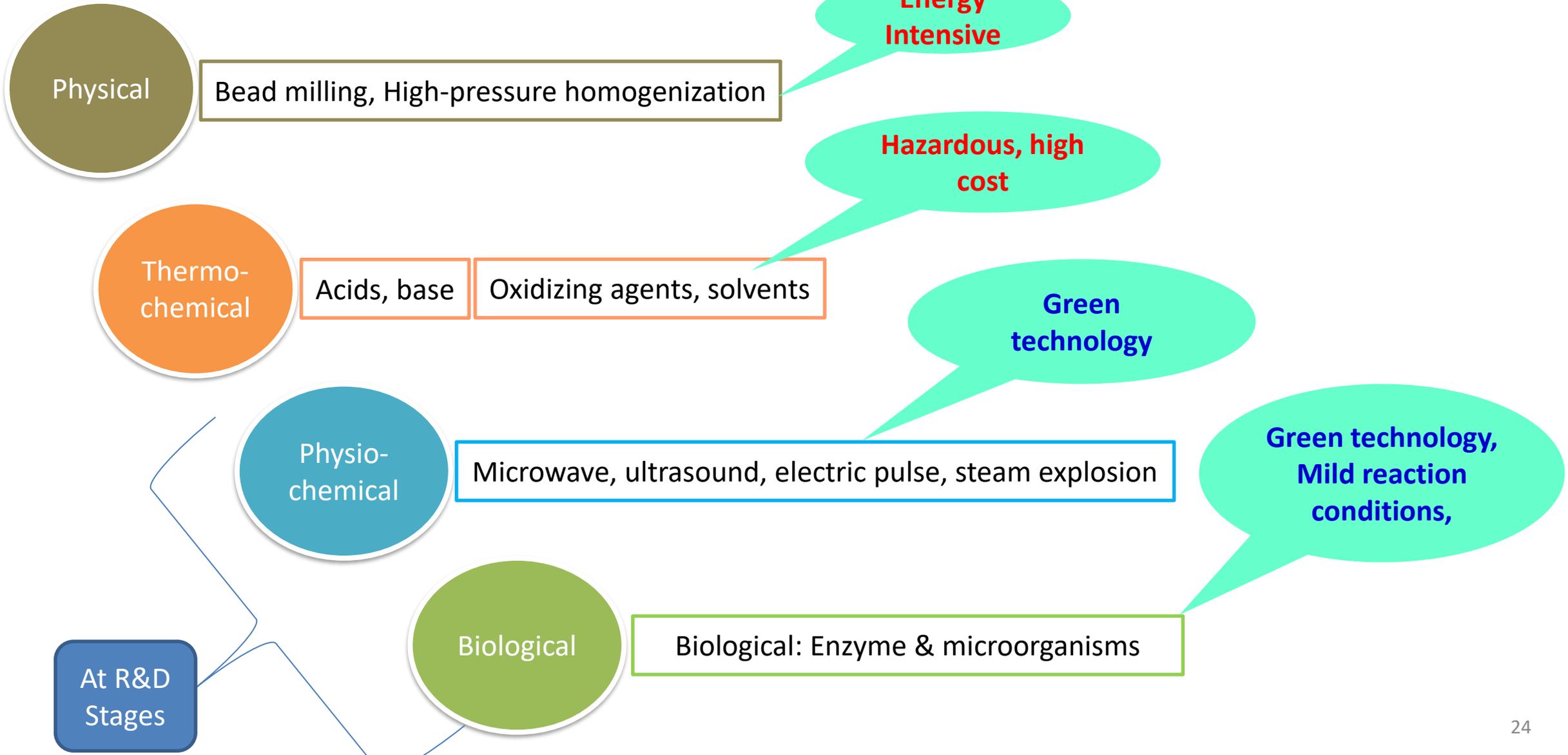
Crystalline

Complex cross-linkage

Recalcitrant

Hard to decompose during anaerobic digestion

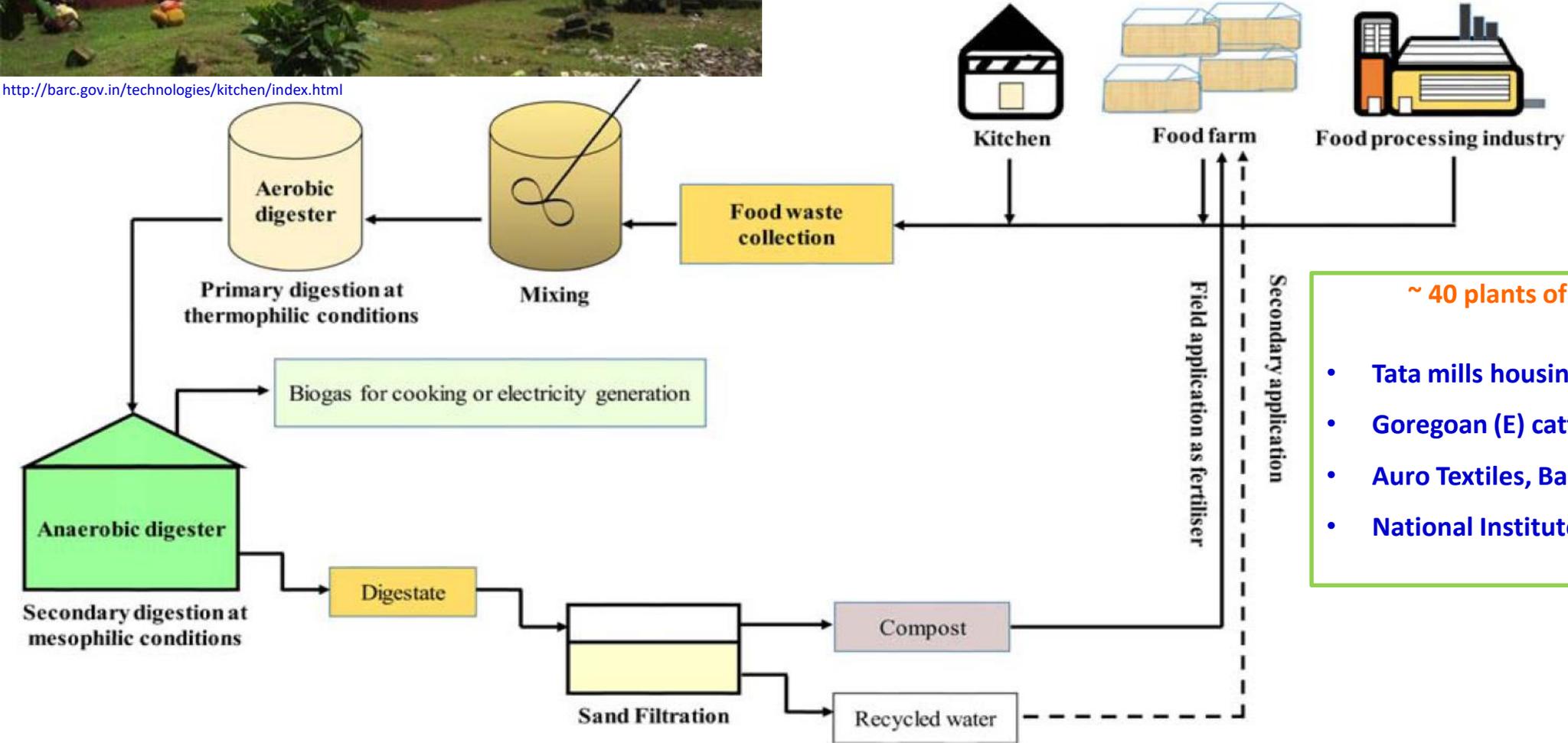
# Pretreatment methods



# Biological pretreatment



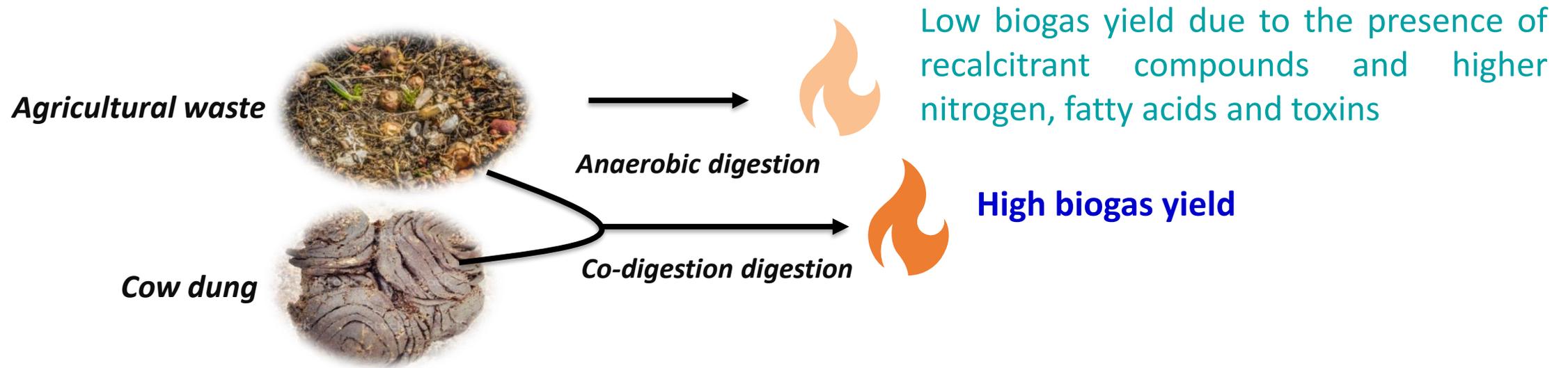
<http://barc.gov.in/technologies/kitchen/index.html>



~ 40 plants of 1-5 TPD commissioned

- Tata mills housing society, Mumbai, INDIA
- Goregoan (E) cattle farm, Mumbai, INDIA
- Auro Textiles, Baddi, INDIA
- National Institute of Technology, Trichy, INDIA

# Co-digestion of substrates



- Co-digestion of the biomass with a high carbonic substrate (high C:N ratio)
- Co-digestion with substrates -----facilitate hydrolysis as well as balance the C/N ratio, inhibitors, pH, and total solid (TS) content.
- Co-digestion aids in reducing ammonia inhibition, along with enhancing biogas production from the feedstock by increasing its digestibility

# ➤ Biogas production through co-digestion in Fazilka, Punjab, India

1500 tons rice straw per year

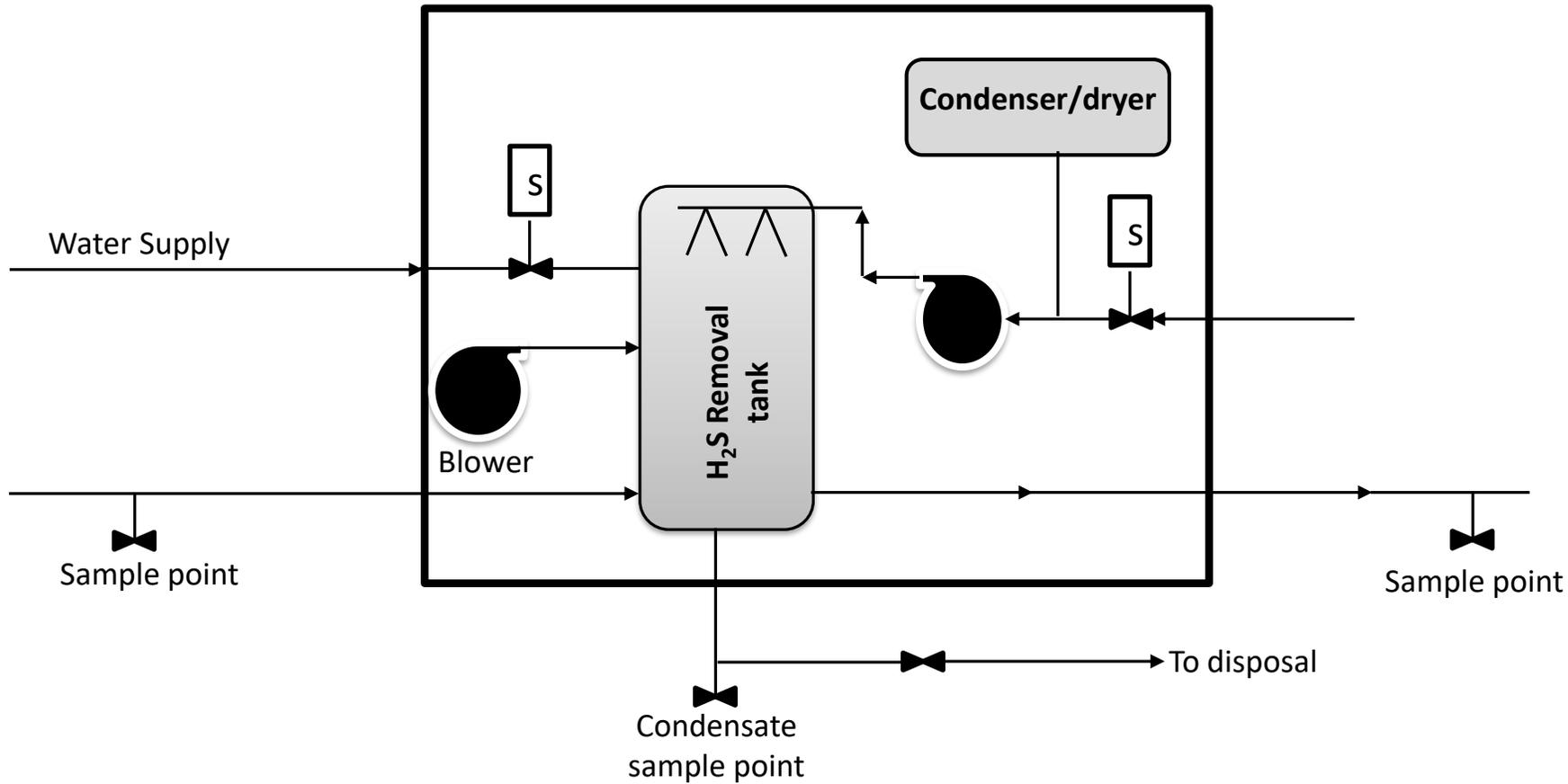
Self consumption 3 MWh per day



# Biogas purification



# H<sub>2</sub>S Removal



<https://www.slb.com/>



granular iron oxide-based H<sub>2</sub>S adsorbent



mixed metal oxide-based H<sub>2</sub>S adsorbents

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## Biological methods for H<sub>2</sub>S removal

i. Chemotrophic and

ii. Photosynthetic

➤ End products are non-hazardous : Sulphur or sulphate

➤ The Sulphur can be utilized as a raw material to produce

- Sulphuric acid,
- Sulphur fertilizers and fungicides used in industry and agriculture

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## i. Chemotrophic method

### ➤ Microbial biodegradation of H<sub>2</sub>S

- Chemotrophic Sulphur oxidizing bacteria

- E.g.-*Thiobacillus, Acidithiobacillus, Sulfolobus, Thiovulum, Thiothrix and Thiospira*
- Utilized Sulphur compounds (e.g. sulphide, polysulphide, elemental sulphur, thiosulphate, sulphite) as chemical energy source , and
- CO<sub>2</sub> as Carbon source

## ii. Photosynthetic separation

### ➤ Purple sulphur bacteria, cyanobacteria, phototrophic members of phylum chloroflexi and heliobacteria and anoxygenic phototrophic sulphur bacteria

- Utilized light as an energy source
- Purple and green sulphur bacteria use reduced sulphur compounds as electron donors for photosynthetic CO<sub>2</sub> reduction

# Conclusion and Process Outlook

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- Biomass pretreatment is crucial to improve the biogas productivity.
- Co-digestion with suitable biomass may facilitate enhanced biogas productivity by reducing ammonia inhibition.
- Maintaining temperature in winters should be looked carefully.
- Rational selection of biogas upgrading technology is indispensable in accordance to capital cost, available land and water resources and biogas application.
- Effective management of digestate slurry may improve the overall process economics.

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*Thank you*

